It-A. End-to-End Process Integration: Successful advances in biochemical processes and the biorefinery concept are co-dependent. This biorefinery concept encompasses a wide range of technical issues related to collecting, storing, transporting, and processing diverse feedstocks, as well as the complexity of integrating several innovative process steps, thus entailing considerable technical risk. The challenge of feed-to-product process integration is crucial, as it impacts both performance and profitability.

It-B. Commercial-Scale Demonstration Facilities: As with all new process technologies, demonstrating sustained integrated performance that meets technical, environmental and safety requirements at sufficiently large scale is an essential step toward commercialization. Demonstration facilities that are capable of testing and validating new technologies and integrated systems are critical to successful commercial deployment. Additionally, increased understanding of these combined systems will result in the optimization of process configurations. Integrating new bioenergy processes with existing biorefineries, while improving the efficiency of all biorefineries, are two critical areas of focus for the platform.

It-C. Risk of Pioneer Technology: The first biorefineries will incorporate a variety of new technologies. The number of new process steps implemented in a demonstration project has been shown to be a strong predictor of future performance shortfalls. Heat and mass balances, and their implications, are not likely to be well understood in regard to new technologies. In addition, the impact of unanticipated buildup of impurities in process streams that can result in abrasion and corrosion of plant equipment and deactivation of process catalysts is not well understood.

It-D. Sensors and Controls: Effective process control will be needed to maintain plant performance and emissions at target levels because of variability in processing conditions, load, feedstock and intermediate stream properties. Development of new sensors and analytical instruments is needed to optimize control systems for biochemical and thermochemical systems. There are several key technical barriers to consider, including the lack of real-time sensors for measuring feedstock moisture and composition, the need for better tools to analyze various process streams, and the lack of process control systems for reactor systems and subsystems.

It-E. Engineering Modeling Tools: The current level of understanding regarding fuels chemistry is insufficient for optimization, scale-up, and commercialization. In order to better understand how fuel chemistry affects commercial viability, rigorous engineering computational fluid dynamic models are needed. Engineering modeling tools are also needed to address heat integration issues.

Biofuels Distribution and End Use

Dm-A. Lack of Biofuels Distribution Infrastructure: The lack of infrastructure to transport, store and dispense biofuels puts biofuels at a disadvantage compared to conventional fuels that already have mature infrastructure. Today's biofuels distribution infrastructure, which includes about 1,000 E85 fueling stations, is concentrated in the Midwest, near the feedstocks (corn and soybeans) and ethanol and biodiesel production facilities. To contribute significantly to the 20 in 10 volumetric goal, expansion beyond this region of the country will be required.

Dm-B. Availability of Biofuels-Compatible Vehicles: About six million ethanol FFVs have been manufactured for the U.S. market, at a price competitive with conventional vehicles. However, at this time, only a limited number of vehicle model/fuel type combinations exist. In addition, most FFVs on the road today use less than 4 gallons of E85 per year due to the limited number of E85 pumps across the U.S.

Dm-C. Industry and Consumer Acceptance and Awareness: To be successful in the marketplace, biomass-derived products must perform at the same level or better than the existing fossil-energy-based products. Industry partners and consumers must believe in the quality, value and safety of biomass-derived products and their benefits.

Dt-A. Ethanol Pipeline Distribution Issues: Ethanol is a stronger solvent than the petroleum products moved via pipeline today. Consequently, ethanol will remove water, rust, gums and other contaminants from the existing petroleum pipeline distribution system. This downgrades the value of the delivered ethanol and adds back-end costs to restore the fuel to meet specifications. Construction of new dedicated ethanol pipelines are limited by the high cost of capital investment, insufficient ethanol supplies, materials compatibility issues, technologies that can measure quality in real time, and existing right-of-way agreements.

Dt-B. Limited Information Available for Developing Codes and Standards: National organizations that develop codes and standards recognize that additional date is required to integrate biofuels into the model codes for infrastructure construction. Thousands of local code jurisdictions in the U.S. adopt and modify these model codes for use in their jurisdictions. At this time, insufficient technical information hinders revision of various codes and standards in support of the quickly accelerating biofuels industry. Lack of codes as well as costly project permitting processes can stymie the introduction of new technologies, including infrastructure, into the marketplace.

Dt-C. Materials Compatibility Issues of Alcohol Fuels: Alcohol fuels and alcohol fuel blends require components throughout the infrastructure system (e.g., fuel storage, pipes and piping, and on-board vehicle systems) that are compatible with the higher electrical conductivity and solubility of the fuel. Higher cost materials, including stainless steel, lined fiberglass tanks, and mild steel with epoxy coatings, are often required to ensure compatibility and mitigate risk of decay or failure.

Dt-D. Increased Evaporative Hydrocarbon Emissions of Ethanol Blends: Adding ethanol to gasoline increases the fuel volatility, as measured by its Reid vapor pressure (RVP). The higher RVP results in higher evaporative hydrocarbon emissions from ethanol blends than from straight gasoline. Ethanol in gasoline also increases the permeability of plastic on-board fuel tanks, which in turn contributes to increased evaporative emissions.

Dt-E. Ethanol Blend Vehicle Fuel Economy: Since ethanol has a lower heating value than gasoline (83,000 Btu/gal for E85 vs. 113,500 Btu/gal for gasoline), E85 delivers a lower fuel economy when compared to gasoline on a gallon by gallon basis. Lower fuel economy can be counteracted by optimizing the engine design to take advantage of the higher octane rating of E85 (98 for E85 vs. 87 for gasoline).

Sustainability

St-A. Climate: Reduce greenhouse gas emissions associated with biofuel production, conversion and use, in comparison to fossil fuels.

St-B. Soil Health and Agronomics: Maintain or improve soil quality and land productivity.

St-C. Water Quality and Quantity: Increase water re-use efficiency and maintain or improve water quality.

St-D. Air Quality: Maintain or improve air quality by reducing the emissions of harmful pollutants such as SO2, NOx, and aromatic compounds.

St-E. Biological Diversity: Conserve biological diversity.

St-F. Land Use: Minimize negative land use change impacts domestically and globally.

St-G. Efficiency and Productivity: Enhance efficient use of nonrenewable resources and recovery of resources; maximize conversion efficiency and productivity.

St-H. Profitability: Lower production costs.

St-I. Rural Development: Enhance economic welfare and rural development through job creation and income growth.

St-J. Standards: Develop standards and corresponding metrics for ensuring sustainable biofuel production globally.

St-K. Energy Diversification and Security: Reduce dependence on foreign oil and increase energy supply diversity.

St-L. Net Energy Balance: Ensure positive net energy balance for all alternatives to fossil fuels.

1. Wet Mill Improvements Pathway	
Milestone #	**Milestone Title**
M.1	***Complete systems level demonstration and validation of technologies to improve corn wet mill facilities using corn grain feedstock***
M.1.1	Demonstrate and validate economical residual starch conversion in a wet mill
M.1.1.1	Convert residual starch in fiber stream to EtOH
M.1.1.2	Evaluate new feed product
M.1.1.3	Validate integrated process at pilot scale
M.1.1.4	Validate new process in wet mill
M.1.2	Demonstrate and validate economical fiber conversion to C5 and/or mixed C5/C6 sugars in a wet mill (residual starch also expected to be converted during fiber processing)
M.1.2.1	Solubilize hemicellulose in fiber to C5 sugars
M.1.2.2	Hydrolyze cellulose to C6 Sugar
M.1.2.3	Validate integrated process at pilot scale
M.1.2.4	Evaluate new feed product
M.1.2.5	Validate new process in wet mill
M.1.3	Demonstrate and validate economical conversion of mixed sugars to ethanol in a wet mill
M.1.3.1	Convert released sugars to ethanol
M.1.3.2	Validate integrated process at pilot scale
M.1.3.3	Validate new process in wet mill
M.1.4	Demonstrate and validate economical new products from C5 or mixed C5/C6 sugars in a wet mill
M.1.4.1	Convert released C5 sugars to products
M.1.4.2	Convert C5 sugars to building block chemicals
M.1.4.3	Convert mixed sugars to products
M.1.4.4	Convert mixed sugars to building block chemicals
M.1.4.5	Convert building block chemicals to products
M.1.4.6	Demonstrate product separation and recovery specification
M.1.4.10	Validate integrated process at pilot scale
M.1.4.11	Validate new process in wet mill
M.1.5	Demonstrate and validate economical new products from C6 sugars in a wet mill
M.1.5.1	Convert C6 sugars to products
M.1.5.2	Convert C6 sugars to building block chemicals
M.1.5.3	Convert building block chemicals to products
M.1.5.4	Demonstrate product separation and recovery specification
M.1.5.5	Validate integrated process at pilot scale
M.1.5.6	Validate new process in wet mill
M.1.6	Demonstrate and validate economical new products from corn-derived oils in a wet mill
M.1.6.1	Convert corn derived oils to products
M.1.6.2	Demonstrate product separation and recovery specification
M.1.6.3	Validate integrated process at pilot scale
M.1.6.4	Validate new process in wet mill
2. Dry Mill Improvements Pathway	
Milestone #	**Milestone Title**
M.2	***Complete systems level demonstration and validation of technologies to improve corn dry mill facilities using corn (or other) grain feedstock***

M.2.1	Demonstrate and validate economical residual starch conversion in a dry mill
M.2.1.1	Conversion of residual starch to glucose
M.2.1.2	Evaluate new feed product
M.2.1.3	Conversion of converted glucose to ethanol
M.2.1.4	Validate integrated process in a dry mill
M.2.2	Demonstrate and validate economical fiber conversion in a dry mill (residual starch also expected to be converted during fiber processing)
M.2.2.1	Convert fiber to monomer sugars
M.2.2.2	Evaluate new feed product
M.2.2.3	Validate integrated process at pilot scale
M.2.2.4	Validate new process in dry mill
M.2.3	Demonstrate and validate economical conversion of mixed sugars to ethanol in a dry mill
M.2.3.2	Convert released sugars to ethanol
M.2.3.4	Validate integrated process at pilot scale
M.2.3.5	Validate new process in dry mill
MI.1	Demonstrate and validate economical corn fiber-to-ethanol in a dry mill.
M.2.4	Demonstrate and validate economical conversion of mixed sugars to products in a dry mill
M.2.4.1	Conversion targets from C6 sugars to building blocks
M.2.4.2	Conversion targets from building blocks to products
M.2.4.3	Demonstrate product separation and recovery specification
M.2.4.4	Validate integrated process at pilot scale
M.2.4.5	Validate new process in dry mill
M.2.5	Demonstrate and validate economical new products from C6 sugars in a dry mill
M.2.5.1	Conversion targets from C6 sugars to building blocks
M.2.5.2	Conversion targets from building blocks to products
M.2.5.3	Product separation specification
M.2.5.4	Validate integrated process at pilot scale
M.2.5.5	Validate new process in dry mill
M.2.6	Demonstrate and validate economical front end fractionation processes in a dry mill
M.2.6.1	Derive additional value added products from front end fractionation
M.2.6.2	Evaluate new feed coproducts
M.2.6.3	Validate integrated process at pilot scale
M.2.6.4	Validate new process in dry mill
M.2.7	Investigate alternate sources for dry mill heat and power
M.2.7.1	Thermochemical processing of fiber stream to heat, power
M.2.7.2	Thermochemical processing of residues (i.e. corn stover) to heat, power
M.2.7.3	Validate integrated process at pilot scale
M.2.7.4	Validate new process in dry mill
3. Oil Mill Improvements Pathway	
Milestone #	**Milestone Title**
M.3	***Complete systems level demonstration and validation of technologies to improve oil processing mill facilities***
M.3.1	Demonstrate and validate economical and sustainable new oil crop production for production of biodiesel and other renewable diesel alternatives
M.3.1.1	Demonstrate sustainable agronomic practices
M.3.1.2	Demonstrate oil crop harvesting

M.3.1.3	Demonstrate oil crop storage
M.3.1.4	Demonstrate oil crop transportation
M.3.1.5	Demonstrate quality and quantity of oil crop available
M.3.1.6	Validate integrated oil crop logistics at pilot scale
M.3.1.7	Validate integrated oil crop logistics at demonstration scale
M.3.2	Demonstrate and validate economical new products from glycerol in a natural oil processing facility
M.3.2.1	Convert glycerol to products
M.3.2.2	Recover new products
M.3.2.3	Validate integrated process at pilot scale
M.3.2.4	Validate integrated process in natural oil processing facility
M.3.3	Demonstrate and validate economical new fuels from oils in natural oil processing facility
M.3.3.1	Convert oil to fuels
M.3.3.2	Recover fuels
M.3.3.3	Validate integrated process at pilot scale
M.3.3.4	Validate integrated process in natural oil processing facility
M.3.4	Demonstrate and validate economical new products from oils in natural oil processing facility
M.3.4.1	Convert oil to products
M.3.4.2	Convert oils to building block chemicals
M.3.4.3	Convert building block chemicals to products
M.3.4.4	Recover new products
M.3.4.5	Validate integrated process at pilot scale
M.3.4.6	Validate integrated process in natural oil processing facility
M.3.5	Demonstrate and validate economical cleanup of waste fats and greases for fuel production
M.3.5.1	Validate cleanup performance
M.3.5.2	Validate integrated cleanup at pilot scale
M.3.5.3	Validate integrated process in natural oil processing facility
4. Agricultural Residue Processing Pathway	
Milestone #	**Milestone Title**
M.4	***Complete systems level demonstration and validation of all key technologies to utilize agricultural residue feedstocks in existing or new facilities***
JI.2007	Complete preliminary engineering design package, market analysis, and financial projedctionfor at least two industrial-scale projects consistent with EPAct 2005 requirements.
JI.2008	Approve a final engineering design package of at least one commercial scale biorefinery (up to 700 metric tons per day of feedstock) including findings from an independent engineering review.
JI.2009	Complete engineering design package, market analysis and finanical projections for at least one industrial-scale biorefinery (1-3 MGY).
JI.2009	Initiate construction of at least one commerical-scale biorefinery project (700 tons/day feedstock) including hard orders for all tangible equiopment, vendor packages and structural steel.
JI.2010	Complete commissioning and preliminary operation of at least one commercial-scale biorefinery project (700 tons/day feedstock processed)
JI.2011	Complete constuction, mechanical completion, and commissioning of a 10% industrial scale biorefinery (1-3 million gallons/year) in support of nth plant economics at $1.31 (2007$) per gallon of ethanol by 2012.
JI.2011	Validate economics, system performance, of at least one commercial-scale biorefinery project (700 tons/day feedstock processed) awarded in FY2007 in support of nth plant economics at $1.31 per gallon of ethanol by 2012. (2007$)
JI.2012	Using commercial scale biorefinery and 10% industrial-scale biorefinery performance, validate nth plant economics at the $1.31/gal ethanol (2007$).

MI.6	Demonstrate and validate integrated agricultural residues-to-ethanol process at demonstration or commercial scale (Biochemical route)
MI.19	Demonstrate and validate production of ethanol from mixed alcohols produced from agricultural residues-derived syngas at demonstration or commercial scale.
JF.2008	Conduct replicated field trials across regions to determine the impact of residue removal on grain yield, and energy crops to assuess resource supply cost and potential and to optimize biorefinery location
JF.2009	Implement a GIS-based regional feedstock atlas system linked to the lateste National Agricultural Statistic Service data, energy crop field test resultes and residue removal trial results
JF.2010	Complete a core R&D engineering design that can receive multiple feedstock resources and preprocess them into cellulosic feedstock for an average of $35 per ton delivered to biorefineries.
JF.2011	In conjunction with USDA, land grant universities, and private sector, incorporate yield and othe data from field trials. Complete and validate dry and woody feedstocks at $35 per ton in line with 2012 goal.
JF.2012	Feedstocks (wet, dry, and woody) in support of $1.07 per gallon cost target will be validated on a regional basis.
M.4.1	Demonstrate and validate integrated corn stover harvesting logistics
M.4.1.1	Demonstrate sustainable corn agronomic practices that account for corn stover harvesting
M.4.1.2	Demonstrate wet and dry corn stover harvesting
M.4.1.3	Demonstrate wet and dry corn stover storage
M.4.1.4	Demonstrate wet and dry corn stover transportation
M.4.1.5	Demonstrate wet and dry quality and quantity of corn stover available
M.4.1.6	Demonstrate corn stover preprocessing benefits
M.4.1.7	Validate integrated corn stover logistics in prototype equipment
M.4.1.8	Validate integrated corn stover logistics at demonstration scale
M.4.2	Demonstrate and validate integrated wheat straw harvesting logistics
M.4.2.1	Demonstrate sustainable wheat agronomic practices that account for wheat straw harvesting
M.4.2.2	Demonstrate wet and dry wheat straw harvesting
M.4.2.3	Demonstrate wet and dry wheat straw storage
M.4.2.4	Demonstrate wet and dry wheat straw transportation
M.4.2.5	Demonstrate wet and dry quality and quantity of wheat straw available
M.4.2.6	Demonstrate wheat straw preprocessing benefits
M.4.2.7	Validate integrated wheat straw logistics in prototype equipment
M.4.2.8	Validate integrated wheat straw logistics at demonstration scale
M.4.3	Demonsrate and validate integrated rice straw harvesting logistics
M.4.3.1	Demonstrate sustainable rice agronomic practices that account for rice straw harvesting
M.4.3.2	Demonstrate wet and dry rice straw harvesting
M.4.3.3	Demonstrate wet and dry rice straw storage
M.4.3.4	Demonstrate wet and dry rice straw transportation
M.4.3.5	Demonstrate wet and dry quality and quantity of rice straw available
M.4.3.6	Demonstrate rice straw preprocessing benefits
M.4.3.7	Validate integrated rice straw logistics in prototype equipment
M.4.3.8	Validate integrated rice straw logistics at demonstration scale
M.4.4	Feedstock FlexIbility and Availability via Blending Depot or Elevator
M.4.4.1	To be determined
M.4.5	Demonstrate and validate ag residue fractionation to produce mixed, dilute biomass sugars
M.4.5.1	Validate cellulase enzyme cost
M.4.5.2	Validate pretreatment technology cost

M.4.5.3	Demonstrate ability to economically satisfy internal heat and power demands
M.4.5.4	Validate capital cost
M.4.5.5	Validate integrated pretreatment and enzymatic hydrolysis at pilot scale
M.4.5.6	Validate integrated pretreatment and enzymatic hydrolysis at demonstration scale
M.4.5.7	Validate feed flexibility in integrated system
M.4.6	Demonstrate and validate ethanol from 5 biomass sugars
M.4.6.1	Validate fermentation of all 5 sugars to produce ethanol
M.4.6.2	Optimize ethanol separation
M.4.6.3	Optimize integrated production of ethanol from sugars at pilot scale
M.4.6.4	Optimize integrated production of ethanol from sugars at demonstration scale
JB.2007	Complete integrated tests of pretreatment and enzymatic hydrolysis in conjunction with existing fermentation organisms at bench scale on corn stover that validate the $0.125 per pound sugars on the pathway to achieving $0.064 per pound in 2012.
JB.2010	Achieve 85% xylan-to-xylose conversion with chemical and/or enzymatic hydrolysis that contribute, via increased ethanol yield, to the $1.31 per gallon (2007$) selling price.
JB.2011	Data from integrated runs of pretreatment and enzymatic hydrolysis at lab scale combined with a process design and cost estimate validates that an integrated biorefinery potentially could produce ethanol at a $1.31 per gallon (2007$) selling price
MB.14	Validate integrated corn stover-to-ethanol pilot operation
JB.2012	Data from integrated pilot operation combined with process design and cot estimate validates a $1.31 per gallon (2007$) selling price.
M.4.7	Demonstrate and validate chemical building blocks, chemicals or materials from 5 biomass sugars
M.4.7.1	Optimize chemical building blocks production
M.4.7.2	Optimize high value chemical production
M.4.7.3	Optimize product separation
M.4.7.4	Optimize integrated production of product(s) from sugars at pilot scale
M.4.7.5	Optimize integrated production of product(s)from sugars at demonstration scale
M.4.8	Demonstrate and validate high value chemical and material products from lignin intermediates
M.4.8.1	Demonstrate high value chemical/material production from lignin
M.4.8.2	Validate product separation
M.4.8.3	Validate integrated production of product(s)from lignin at pilot scale
M.4.8.4	Validate integrated production of product(s)from lignin at demonstration scale
M.4.9	Demonstrate and validate fuel products from lignin intermediates
M.4.9.1	Demonstrate direct fuel production from lignin
M.4.9.2	Validate fuel product separation
M.4.9.3	Validate integrated production of fuel(s)from lignin at pilot scale
M.4.9.4	Validate integrated production of fuels(s)from lignin at demonstration scale
M.4.10	Demonstrate and validate combined heat and power from lignin intermediates/residues
M.4.10.1	Demonstrate combined heat and power production from lignin
M.4.10.2	Validate integrated production of heat and power from lignin at pilot scale
M.4.10.3	Validate integrated production of heat and power from lignin at demonstration scale
M.4.11	Demonstrate and validate lignin gasification to produce syngas
M.4.11.1	Validate feeder system performance
M.4.11.2	Validate gasification performance
M.4.11.3	Validate gas cleanup performance
M.4.11.4	Validate capital costs
M.4.11.5	Validate integrated gasification and gas cleanup at pilot scale

M.4.11.6	Validate integrated gasification and gas cleanupat demonstration scale
M.4.12	Demonstrate and validate biomass gasification to produce syngas
M.4.12.1	Validate feeder systems to reliably feed solid biomass to high pressure (30 bar) systems
M.4.12.2	Validate gasification performance
M.4.12.3	Validate gas cleanup performance
M.4.12.4	Validate capital costs
M.4.12.5	Validate integrated gasification and gas cleanup at pilot scale
M.4.12.6	Validate integrated gasification and gas cleanupat demonstration scale
M.4.12.7	Validate feed flexibility in integrated system
JT.2007	Demonstrate conversion of 50% of non-methane (C2+ higher) hydrocarbons that result in a syngas cost of $7.15/MBtu in 2007.
JT.2009	Validate technology capable of economically converting biomass residues, pulping liquors or waste fats and greases to synthesis gas or bio-oils that are suitable for fuels and chemicals produciton. The target is a modeled cost of $5.81/Mbtu in 2009.
JT.2010	Validate and demonstrate technology for the cost-effective cleanup of biomass synthesis gas leading to a modeled syngas cost of $5.40/Mbtu in 2010.
M.4.13	Demonstrate and validate ethanol from mixed alcohols using lignin or biomass derived syngas
M.4.13.1	Demonstrate ethanol production from mixed alcohols
M.4.13.2	Validate ethanol separation
M.4.13.3	Validate integrated production of ethanol from syngas at pilot scale
M.4.13.4	Validate integrated production of ethanol from syngas at demonstration scale
MT.19	Validate integrated corn stover/wheat straw-to-ethanol (via gasification) pilot operation.
M.4.14	Demonstrate and validate hydrogen production from lignin or biomass derived syngas
M.4.14.1	Demonstrate optimized hydrogen production from syngas
M.4.14.2	Validate hydrogen separation/recovery
M.4.14.3	Validate integrated production of hydrogen from syngas at pilot scale
M.4.14.4	Validate integrated production of hydrogen from syngas at demonstration scale
M.4.15	Demonstrate and validate combined heat and power production from lignin or biomass derived syngas
M.4.15.1	Demonstrate combined heat and power production from syngas
M.4.15.2	Validate integrated production of heat and power from syngas at pilot scale
M.4.15.3	Validate integrated production of heat and power from syngas at demonstration scale
M.4.16	Demonstrate and validate non-ethanol fuels from lignin or biomass derived syngas
M.4.16.1	Demonstrate non-ethanol fuel production from lignin or biomass-derived syngas
M.4.16.2	Validate non-ethanol fuel separation
M.4.16.3	Validate integrated production of non-ethanol fuels from syngas at pilot scale
M.4.16.4	Validate integrated production of non-ethanol fuels from syngas at demonstration scale
M.4.17	Demonstrate and validate product(s) from lignin or biomass derived syngas
M.4.17.1	Demonstrate high value chemical/material production (C3-C5 alcohols) from syngas
M.4.17.2	Validate product(s) separation
M.4.17.3	Validate integrated production of product(s) from syngas at pilot scale
M.4.17.4	Validate integrated production of product(s) from syngas at demonstration scale
M.4.18	Demonstrate and validate non-ethanol fuels from 5 biomass sugars that are econonomically viable
M.4.18.1	Validate fermentation of all 5 sugars to produce non-ethanol fuels
M.4.18.2	Optimize non-ethanol fuel separation
M.4.18.3	Optimize integrated production of non-ethanol fuels from sugars at pilot scale
M.4.18.4	Optimize integrated production of non-ethanol fuel from sugars at demonstration scale

M.4.19	Demonstrate and validate biomass pyrolysis to produce pyrolysis oil intermediate
M.4.19.1	Validate feeder systems to reliably feed solid biomass to pyrolysis reactor high pressure (30 bar) systems
M.4.19.2	Validate pyrolysis performance
M.4.19.3	Validate pyrolysis oil cleanup performance
M.4.19.4	Validate capital costs - ROI hurdle rate versus cost magnitude hurdle amount
M.4.19.5	Validate integrated pyrolysis and pyrolysis oil cleanup at pilot scale
M.4.19.6	Validate integrated pyrolysis and pyrolysis oil cleanup at demonstration scale
M.4.19.7	Validate feed flexibility in integrated system
M.4.20	Demonstrate and validate fuels from pyrolysis oil intermediate
M.4.20.1	Demonstrate fuel production from pyrolysis oil intermediate
M.4.20.2	Validate fuel separation
M.4.20.3	Validate integrated production of fuels from pyrolysis oil at pilot scale
M.4.20.4	Validate integrated production of fuels from pyrolysis oil at demonstration scale
M.4.21	Demonstrate and validate high value chemical and material products from pyrolysis oil intermediates
M.4.21.1	Demonstrate high value chemical/material production from pyrolysis oil
M.4.21.2	Validate product separation
M.4.21.3	Validate integrated production of product(s)from pyrolysis oil at pilot scale
M.4.21.4	Validate integrated production of product(s)from pyrolysis oil at demonstration scale
5. Perennial Crop Processing Pathway Milestones	
Milestone #	**Milestone Title**
M.5	***Complete systems level demonstration and validation of all key technologies to utilize perennial crops in existing or new facilities***
JF.2008	Conduct replicated field trials across regions to determine the impact of residue removal on grain yield, and energy crops to assuess resource supply cost and potential and to optimize biorefinery location
JF.2009	Implement a GIS-based regional feedstock atlas system linked to the latest National Agricultural Statistic Service data, energy crop field test resultes and residue removal trial results
JF.2010	Incorporate new varieties/clones developed at land grants, universities and private sector into regionally-based field trial sites. Update GIS system with new information obtained from trials and initiate new trials for post-2012 timeframe.
JF.2010	Complete a core R&D engineering design that can receive multiple feedstock resources and preprocess them into cellulosic feedstock for an average of $35 per ton delivered to biorefineries.
JF.2011	In conjunction with USDA, land grant universities, and private sector, incorporate yield and othe data from field trials. Complete and validate dry and woody feedstocks at $35 per ton in line with 2012 goal.
JF.2012	Feedstocks (wet, dry, and woody) in support of $1.07 per gallon cost target will be validated on a regional basis.
M.5.1	Demonstrate and validate integrated switchgrass production and harvesting logistics
M.5.1.1	Demonstrate sustainable switchgrass agronomic practices
M.5.1.2	Demonstrate wet and dry switchgrass harvesting
M.5.1.3	Demonstrate wet and dry switchgrass storage
M.5.1.4	Demonstrate wet and dry switchgrass transportation
M.5.1.5	Demonstrate quality and quantity of switchgrass available
M.5.1.6	Demonstrate switchgrass prepprocessing benefits
M.5.1.7	Validate integrated switchgrass logistics in prototype equipment
M.5.1.8	Validate integrated switchgrass logistics at demonstration scale
M.5.2	Demonstrate and validate integrated woody crop harvesting logistics
M.5.2.1	Demonstrate sustainable woody crop agronomic practices
M.5.2.2	Demonstrate woody crop harvesting

M.5.2.3	Demonstrate woody crop storage
M.5.2.4	Demonstrate woody crop transportation
M.5.2.5	Demonstrate quality and quantity of woody crops available
M.5.2.6	Demonstrate woody crop preprocessing benefits
M.5.2.7	Validate integrated woody crop logistics in prototype equipment
M.5.2.8	Validate integrated woody crop logistics at demonstration scale
M.5.3	Feedstock FlexIbility and Availability via Blending Depot or Elevator
M.5.3.1	To be determined
M.5.4	Demonstrate and validate switchgrass fractionation to produce mixed biomass sugars
M.5.4.1	Validate cellulase enzyme cost
M.5.4.2	Validate pretreatment technology cost
M.5.4.3	Demonstrate ability to economically satisfy internal heat and power demands
M.5.4.4	Validate capital cost
M.5.4.5	Validate integrated pretreatment and enzymatic hydrolysis at pilot scale
M.5.4.6	Validate integrated pretreatment and enzymatic hydrolysis at demonstration scale
M.5.4.7	Validate feed flexibility in integrated system
JB.2008	Achieve a modeled cost target of $0.11 per pound of sugars (equivalent to $2.09 per gallon of cellulosic ethanol) through the formulation of improved enzyme mixtures and pretreatments.
JB.2009	Demonstrate alternative pretreatment technologies integrated with enzymatic hydrolysis at lab scale that have the potential of contributing ot the $1.31 per gallon (2007$) ethanol selling price target in 2012.
M.5.5	Demonstrate and validate woody crop fractionation to produce mixed, dilute biomass sugars
M.5.5.1	Validate cellulase enzyme cost
M.5.5.2	Validate pretreatment technology cost
M.5.5.3	Demonstrate ability to economically satisfy internal heat and power demands
M.5.5.4	Valicate capital cost
M.5.5.5	Validate integrated pretreatment and enzymatic hydrolysis at pilot scale
M.5.5.6	Validate integrated pretreatment and enzymatic hydrolysis at demonstration scale
M.5.5.7	Validate feed flexibility in integrated system
MB.15	Validate integrated switchgrass-to-ethanol pilot operation
M.5.6	Demonstrate and validate ethanol from 5 biomass sugars
M.5.6.1	Validate ethanol production
M.5.6.2	Validate ethanol separation/recovery
M.5.6.3	Validate integrated production of product(s)from sugars at pilot scale
M.5.6.4	Validate integrated production of product(s)from sugars at demonstration scale
M.5.7	Demonstrate and validate products from 5 biomass sugars
M.5.7.1	Validate chemical building blocks production
M.5.7.2	Validate high value chemical production
M.5.7.3	Validate product separation
M.5.7.4	Validate integrated production of product(s)from sugars at pilot scale
M.5.7.5	Validate integrated production of product(s)from sugars at demonstration scale
M.5.8	Demonstrate and validate high value chemical and material products from lignin intermediates
M.5.8.1	Demonstrate high value chemical/material production from lignin
M.5.8.2	Validate product separation
M.5.8.3	Validate integrated production of product(s)from lignin at pilot scale

M.5.8.4	Validate integrated production of product(s)from lignin at demonstration scale
M.5.9	Demonstrate and validate fuel products from lignin intermediates
M.5.9.1	Demonstrate direct fuel production from lignin
M.5.9.2	Validate fuel product separation
M.5.9.3	Validate integrated production of fuel(s)from lignin at pilot scale
M.5.9.4	Validate integrated production of fuels(s)from lignin at demonstration scale
M.5.10	Demonstrate and validate combined heat and power from lignin intermediates/residues
M.5.10.1	Demonstrate combined heat and power production from lignin
M.5.10.2	Validate integrated production of heat and power from lignin at pilot scale
M.5.10.3	Validate integrated production of heat and power from lignin at demonstration scale
M.5.11	Demonstrate and validate lignin gasification to produce syngas
M.5.11.1	Validate feeder system performance
M.5.11.2	Validate gasification performance
M.5.11.3	Validate gas cleanup performance
M.5.11.4	Validate capital costs - ROI hurdle rate versus cost magnitude hurdle amount
M.5.11.5	Validate integrated gasification and gas cleanup at pilot scale
M.5.11.6	Validate integrated gasification and gas cleanup at demonstration scale
M.5.12	Demonstrate and validate biomass gasification to produce syngas
M.5.12.1	Validate feeder systems to reliably feed solid biomass to high pressure (30 bar) systems
M.5.12.2	Validate gasification performance
M.5.12.3	Validate gas cleanup performance
M.5.12.4	Validate capital costs
M.5.12.5	Validate integrated gasification and gas cleanup at pilot scale
M.5.12.6	Validate integrated gasification and gas cleanupat demonstration scale
M.5.12.7	Validate feed flexibility in integrated system
JT.2007	Demonstrate conversion of 50% of non-methane (C2+ higher) hydrocarbons that result in a syngas cost of $7.15/MBtu in 2007.
JT.2010	Validate and demonstrate technology for the cost-effective cleanup of biomass synthesis gas leading to a modeled syngas cost of $5.40/Mbtu in 2010.
M.5.13	Demonstrate and validate ethanol from mixed alcohols using lignin or biomass derived syngas
M.5.13.1	Demonstrate ethanol production from mixed alcohols
M.5.13.2	Validate ethanol separation
M.5.13.3	Validate integrated production of ethanol from syngas at pilot scale
M.5.13.4	Validate integrated production of ethanol from syngas at demonstration scale
MT.20	Validate integrated switchgrass/hybrid poplar-to-ethanol (via gasification) pilot operation.
M.5.14	Demonstrate and validate hydrogen production from lignin or biomass derived syngas
M.5.14.1	Demonstrate optimized hydrogen production from syngas
M.5.14.2	Validate hydrogen separation/recovery
M.5.14.3	Validate integrated production of hydrogen from syngas at pilot scale
M.5.14.4	Validate integrated production of hydrogen from syngas at demonstration scale
M.5.15	Demonstrate and validate combined heat and power production from lignin or biomass derived syngas
M.5.15.1	Demonstrate combined heat and power production from syngas
M.5.15.2	Validate integrated production of heat and power from syngas at pilot scale
M.5.15.3	Validate integrated production of heat and power from syngas at demonstration scale
M.5.16	Demonstrate and validate non-ethanol fuels from lignin or biomass derived syngas

M.5.16.1	Demonstrate non-ethanol fuel production from lignin or biomass-derived syngas
M.5.16.2	Validate non-ethanol fuel separation
M.5.16.3	Validate integrated production of non-ethanol fuels from syngas at pilot scale
M.5.16.4	Validate integrated production of non-ethanol fuels from syngas at demonstration scale
M.5.17	Demonstrate and validate product(s) from lignin or biomass derived syngas
M.5.17.1	Demonstrate high value chemical/material production (C3-C5 alcohols) from syngas
M.5.17.2	Validate product(s) separation
M.5.17.3	Validate integrated production of product(s) from syngas at pilot scale
M.5.17.4	Validate integrated production of product(s) from syngas at demonstration scale
M.5.18	Demonstrate and validate non-ethanol fuels from 5 biomass sugars that are econonomically viable
M.5.18.1	Validate fermentation of all 5 sugars to produce non-ethanol fuels
M.5.18.2	Optimize non-ethanol fuel separation
M.5.18.3	Optimize integrated production of non-ethanol fuels from sugars at pilot scale
M.5.18.4	Optimize integrated production of non-ethanol fuel from sugars at demonstration scale
M.5.19	Demonstrate and validate biomass pyrolysis to produce pyrolysis oil intermediate
M.5.19.1	Validate feeder systems to reliably feed solid biomass to pyrolysis reactor high pressure (30 bar) systems
M.5.19.2	Validate pyrolysis performance
M.5.19.3	Validate pyrolysis oil cleanup performance
M.5.19.4	Validate capital costs - ROI hurdle rate versus cost magnitude hurdle amount
M.5.19.5	Validate integrated pyrolysis and pyrolysis oil cleanup at pilot scale
M.5.19.6	Validate integrated pyrolysis and pyrolysis oil cleanup at demonstration scale
M.5.19.7	Validate feed flexibility in integrated system
M.5.20	Demonstrate and validate fuels from pyrolysis oil intermediate
M.5.20.1	Demonstrate fuel production from pyrolysis oil intermediate
M.5.20.2	Validate fuel separation
M.5.20.3	Validate integrated production of fuels from pyrolysis oil at pilot scale
M.5.20.4	Validate integrated production of fuels from pyrolysis oil at demonstration scale
M.5.21	Demonstrate and validate high value chemical and material products from pyrolysis oil intermediates
M.5.21.1	Demonstrate high value chemical/material production from pyrolysis oil
M.5.21.2	Validate product separation
M.5.21.3	Validate integrated production of product(s)from pyrolysis oil at pilot scale
M.5.21.4	Validate integrated production of product(s)from pyrolysis oil at demonstration scale
	6. Forest Resources Processing
Milestone #	**Milestone Title**
M.6	***Complete systems level demonstration and validation of technologies to improve pulp and paper mill facilities and/or produce additional products (fuels, chemicals and /or power) from wood feedstock in a pulp and paper mill environment***
JF.2010	Complete a core R&D engineering design that can receive multiple feedstock resources and preprocess them into cellulosic feedstock for an average of $35 per ton delivered to biorefineries.
JF.2011	In conjunction with USDA, land grant universities, and private sector, incorporate yield and othe data from field trials. Complete and validate dry and woody feedstocks at $35 per ton in line with 2012 goal.
JF.2012	Feedstocks (wet, dry, and woody) in support of $1.07 per gallon cost target will be validated on a regional basis.
M.6.1	Demonstrate and validate integrated logging residue and forest thinnings collection and logistics
M.6.1.1	Demonstrate sustainable logging practices
M.6.1.2	Demonstrate logging residue collection

M.6.1.3	Demonstrate forest thinnings collection
M.6.1.4	Demonstrate logging residue and forest thinnings transportation
M.6.1.5	Demonstrate quality and quantity of logging residue and forest thinnings available
M.6.1.6	Demonstrate logging residue and forest thinnings preprocessing benefits
M.6.1.7	Validate integrated logging residue and forest thinnings logistics in prototype equipment
M.6.1.8	Validate integrated logging residue and forest thinnings logistics at demonstration scale
M.6.2	Demonstrate and validate integrated fuel treatment biomass collection and logistics
M.6.2.1	Demonstrate fuel treatment biomass collection
M.6.2.2	Demonstrate fuel treatment biomass storage
M.6.2.3	Demonstrate fuel treatment biomass transportation
M.6.2.4	Demonstrate fuel treatment biomass quality and quantity of available
M.6.2.5	Demonstrate fuel treatment biomass preprocessing benefits
M.6.2.6	Validate integrated fuel treatment biomass logistics in prototype equipment
M.6.2.7	Validate integrated fuel treatment biomass logistics at demonstration scale
M.6.3	Demonstrate and validate forest resources fractionation to produce mixed, dilute biomass sugars
M.6.3.1	Validate cellulase enzyme cost
M.6.3.2	Validate pretreatment technology cost
M.6.3.3	Demonstrate ability to economically satisfy internal heat and power demands
M.6.3.4	Validate capital cost
M.6.3.5	Validate integrated pretreatment and enzymatic hydrolysis at pilot scale
M.6.3.6	Validate integrated pretreatment and enzymatic hydrolysis at demonstration scale
M.6.3.7	Validate feed flexibility in integrated system
M.6.4	Demonstrate and validate ethanol from 5 biomass sugars
M.6.4.1	Validate fermentation of all 5 sugars to produce ethanol
M.6.4.2	Optimize ethanol separation
M.6.4.3	Optimize integrated production of ethanol from sugars at pilot scale
M.6.4.4	Optimize integrated production of ethanol from sugars at demonstration scale
M.6.5	Demonstrate and validate non-ethanol fuels from 5 biomass sugars
M.6.5.1	Validate fermentation of all 5 sugars to produce non-ethanol fuels
M.6.5.2	Optimize fuel separation
M.6.5.3	Optimize integrated production of non-ethanol fuels from sugars at pilot scale
M.6.5.4	Optimize integrated production of non-ethanol fuels from sugars at demonstration scale
M.6.6	Demonstrate and validate chemical building blocks, chemicals or materials from 5 biomass sugars
M.6.6.1	Optimize chemical building blocks production
M.6.6.2	Optimize high value chemical production
M.6.6.3	Optimize product separation
M.6.6.4	Optimize integrated production of product(s) from sugars at pilot scale
M.6.6.5	Optimize integrated production of product(s) from sugars at demonstration scale
M.6.7	Demonstrate and validate fuel products from lignin intermediates
M.6.7.1	Demonstrate direct fuel production from lignin
M.6.7.2	Validate fuel product separation
M.6.7.3	Validate integrated production of fuel(s) from lignin at pilot scale
M.6.7.4	Validate integrated production of fuels(s) from lignin at demonstration scale
M.6.8	Demonstrate and validate high value chemical and material products from lignin intermediates

M.6.8.1	Demonstrate high value chemical/material production from lignin
M.6.8.2	Validate product separation
M.6.8.3	Validate integrated production of product(s) from lignin at pilot scale
M.6.8.4	Validate integrated production of product(s) from lignin at demonstration scale
M.6.9	Demonstrate and validate combined heat and power from lignin intermediates/residues
M 6.9.1	Demonstrate combined heat and power production from lignin
M 6.9.2	Validate integrated production of heat and power from lignin at pilot scale
M 6.9.3	Validate integrated production of heat and power from lignin at demonstration scale
M 6.10	Demonstrate and validate lignin gasification to produce syngas
M 6.10.1	Validate feeder system performance
M 6.10.2	Validate gasification performance
M 6.10.3	Validate gas cleanup performance
M 6.10.4	Validate capital cost
M 6.10.5	Validate integrated gasification and gas cleanup at pilot scale
M 6.10.6	Validate integrated gasification and gas cleanup at demonstration scale
M 6.11	Demonstrate and validate cost-effective biomass gasification of wood, forest residues and other process residues and synthesis gas cleanup in a forest resources mill environment
M 6.11.1	Develop cost effective gasification designs for syngas production at appropriate scale
M 6.11.2	Validate feeder system performance to reliably feed solids to high pressure (30 bar) systems)
M 6.11.3	Validate gasification performance
M 6.11.4	Validate cost-effective gas cleanup performance
M 6.11.5	Validate integrated biomass gasification and syngas cleanup process at pilot scale
M 6.11.6	Validate integrated biomass gasification and syngas cleanup process in a forest resources mill environment
	Validate feed flexibility in integrated system
JT.2007	Demonstrate conversion of 50% of non-methane (C2+ higher) hydrocarbons that result in a syngas cost of $7.15/MBtu in 2007.
JT.2009	Validate technology capable of economically converting biomass residues, pulping liquors or waste fats and greases to synthesis gas or bio-oils that are suitable for fuels and chemicals produciton. The target is a modeled cost of $5.81/Mbtu in 2009.
JT.2010	Validate and demonstrate technology for the cost-effective cleanup of biomass synthesis gas leading to a modeled syngas cost of $5.40/Mbtu in 2010.
M 6.12	Demonstrate and validate production of ethanol from syngas in a forest resources mill environment
M 6.12.1	Produce mixed alcohols from syngas
M 6.12.2	Recover ethanol fuel product
M 6.12.3	Validate integrated process at pilot scale
M 6.12.4	Validate new process in a forest resources mill environment
M 6.13	Demonstrate and validate production of non-ethanol fuels from syngas in a forest resources mill environment
M 6.13.1	Produce non-ethanol fuel from biomass syngas
M 6.13.2	Recover fuel product
M 6.13.3	Validate integrated process at pilot scale
M 6.13.4	Validate new process in a forest resources mill environment
M 6.14	Demonstrate and validate hydrogen production from lignin or biomass derived syngas forest resources mill environment
M 6.14.1	Demonstrate optimized hydrogen production from syngas
M 6.14.2	Validate hydrogen separation/recovery
M 6.14.3	Validate integrated production of hydrogen from syngas at pilot scale
M 6.14.4	Validate integrated production of hydrogen from syngas at demonstration scale

M 6.15	Demonstrate and validate product(s) from lignin or biomass derived syngas forest resources mill environment
M 6.15.1	Demonstrate high value chemical/material productionfrom syngas
M 6.15.2	Validate product(s) separation
M 6.15.3	Validate integrated production of product(s) from syngas at pilot scale
M 6.15.4	Validate integrated production of product(s) from syngas at demonstration scale
M 6.16	Demonstrate and validate syngas utilization for combined heat and power in a forest resources mill environment
M 6.16.1	Verify fuel gas quality to levels necessary for CHP or clean cold gas consuming equipment
M 6.16.2	Validate CHP from syngas and/or direct use of sygas in process equipment
M 6.16.3	Validate integrated process at pilot scale
M 6.16.4	Validate new process in a forest resources mill environment
M 6.17	Demonstrate and validate bio-oil production to a stable intermediate forest resources mill environment
M 6.17.1	Validate bio-oil production
M 6.17.2	Validate bio-oil inermediate recovery
M 6.17.3	Validate integrated process for producing bio-oil at pilot scale
M 6.17.4	Demonstrate and validate new process in a forest resources mill environment
M 6.17.5	Validate feed flexibility in integrated system
M 6.18.	Achieve cost-effective conversion bio-oil intermediate into product(s) in a forest resources mill environment
M 6.18.1	Validate production of products from bio-oil
M 6.18.2	Validate bio-oil product(s) recovery
M 6.18.3	Validate integrated process for producing bio-oil product at pilot scale
M 6.18.4	Validate integrated process in a forest resources mill environment
M 6.19.	Achieve cost-effective conversion bio-oil intermediate into product(s) in a forest resources mill environment
M 6.19.1	Validate production of products from bio-oil
M 6.19.2	Validate bio-oil product(s) recovery
M 6.19.3	Validate integrated process for producing bio-oil product at pilot scale
M 6.19.4	Validate integrated process in a forest resources mill environment
M 6.20	Demonstrate and validate cost-effective extraction of C5 and C6 sugars from hemicellulose upstream of the pulp digestor in a pulp mill without negatively impacting paper quality
M 6.20.1	Meet yield target for C5 and C6 sugars without negatively impacting paper quality
M 6.20.2	Meet sugar upgrading requirements
M 6.20.3	Meet targets for recovery of other intermediates
M 6.20.4	Validate integrated sugar extraction process at pilot scale
M 6.20.5	Validate sugar extraction process in pulp and paper mill
M 6.21	Demonstrate and validate reliable and economic gasification of spent pulping liquor, recycle liquor causticization, chemical recovery and gas cleanup in a pulp mill
M 6.21.1	Validate reliable and economic performance of gasification of spent pulping liquor
M 6.21.2	Validate cost effective causticization and return Na based pulping chemicals
M 6.21.3	Validate advantages of co-gasification of spent pulping liquors and other forms of biomass (woody, recycle paper streams, and bio-oil)
M 6.21.4	Validate process chemical recovery from spent pulping liquor syngas
M 6.21.5	Validategas cleanup technologies on spent pulping liquor syngas
M 6.21.6	Validate integrated black liquor gasification, causticization, chemical recovery and gas cleanup process at pilot scale
M 6.21.7	Validate integrated black liquor gasification, causticization, chemical recovery and gas cleanup process in pulp and paper mill
JB.2011	Demonstrate the conversion of synthesis gas or bio-oils, derived from biomass pulping liquors or waste fats and greases to chemicals or transportation fuels. The target modeled cost is $5.25/Mbtu in 2011.

7. Waste Processing Pathway	
Milestone #	**Milestone Title**
M.7	***Complete systems level demonstration and validation of technologies to process waste biomass streams to produce fuels, chemicals and /or power.***
M.7.1	Demonstrate and validate fractionation of carbohydrate rich waste streams to produce mixed, dilute biomass sugars
M.7.1.1	Validate cellulase enzyme cost
M.7.1.2	Validate pretreatment technology cost
M.7.1.3	Demonstrate ability to economically satisfy internal heat and power demands
M.7.1.4	Validate capital cost
M.7.1.5	Validate integrated pretreatment and enzymatic hydrolysis at pilot scale
M.7.1.6	Validate integrated pretreatment and enzymatic hydrolysis at demonstration scale
M.7.1.7	Validate feed flexibility in integrated system
M.7.2	Demonstrate and validate ethanol from 5 biomass sugars
M.7.2.1	Validate fermentation of all 5 sugars to produce ethanol
M.7.2.2	Optimize ethanol separation
M.7.2.3	Optimize integrated production of ethanol from sugars at pilot scale
M.7.2.4	Optimize integrated production of ethanol from sugars at demonstration scale
M.7.3	Demonstrate and validate non-ethanol fuels from 5 biomass sugars
M.7.3.1	Validate fermentation of all 5 sugars to produce non-ethanol fuels
M.7.3.2	Optimize non-ethanol fuel separation
M.7.3.3	Optimize integrated production of non-ethanol fuels from sugars at pilot scale
M.7.3.4	Optimize integrated production of non-ethanol fuel from sugars at demonstration scale
M.7.4	Demonstrate and validate chemical building blocks, chemicals or materials from 5 biomass sugars
M.7.4.1	Optimize chemical building blocks production
M.7.4.2	Optimize high value chemical production
M.7.4.3	Optimize product separation
M.7.4.4	Optimize integrated production of product(s)from sugars at pilot scale
M.7.4.5	Optimize integrated production of product(s)from sugars at demonstration scale
M.7.6	Demonstrate and validate high value chemical and material products from lignin intermediates
M.7.6.1	Demonstrate high value chemical/material production from lignin
M.7.6.2	Validate product separation
M.7.6.3	Validate integrated production of product(s)from lignin at pilot scale
M.7.6.4	Validate integrated production of product(s)from lignin at demonstration scale
M.7.5	Demonstrate and validate fuel products from lignin intermediates
M.7.5.1	Demonstrate direct fuel production from lignin
M.7.5.2	Validate fuel product separation
M.7.5.3	Validate integrated production of fuel(s)from lignin at pilot scale
M.7.5.4	Validate integrated production of fuels(s)from lignin at demonstration scale
M.7.7	Demonstrate and validate combined heat and power from lignin intermediates/residues
M.7.7.1	Demonstrate combined heat and power production from lignin
M.7.7.2	Validate integrated production of heat and power from lignin at pilot scale
M.7.7.3	Validate integrated production of heat and power from lignin at demonstration scale
M.7.8	Demonstrate and validate lignin gasification to produce syngas
M.7.8.1	Validate feeder system performance

M.7.8.2	Validate gasification performance
M.7.8.3	Validate gas cleanup performance
M.7.8.4	Validate capital costs
M.7.8.5	Validate integrated gasification and gas cleanup at pilot scale
M.7.8.6	Validate integrated gasification and gas cleanupat demonstration scale
M.7.9	Demonstrate and validate waste biomass gasification to produce syngas
M.7.9.1	Validate feeder systems to reliably feed solid biomass to high pressure (30 bar) systems
M.7.9.2	Validate gasification performance
M.7.9.3	Validate gas cleanup performance
M.7.9.4	Validate capital costs
M.7.9.5	Validate integrated gasification and gas cleanup at pilot scale
M.7.9.6	Validate integrated gasification and gas cleanupat demonstration scale
M.7.9.7	Validate feed flexibility in integrated system
JT.2009	Validate technology capable of economically converting biomass residues, pulping liquors or waste fats and greases to synthesis gas or bio-oils that are suitable for fuels and chemicals produciton. The target is a modeled cost of $5.81/Mbtu in 2009.
M.7.10	Demonstrate and validate ethanol from mixed alcohols using lignin or waste biomass derived syngas
M.7.10.1	Demonstrate ethanol production from mixed alcohols
M.7.10.2	Validate ethanol separation
M.7.10.3	Validate integrated production of ethanol from syngas at pilot scale
M.7.10.4	Validate integrated production of ethanol from syngas at demonstration scale
JB.2011	Demonstrate the conversion of synthesis gas or bio-oils, derived from biomass pulping liquors or waste fats and greases to chemicals or transportation fuels. The target modeled cost is $5.25/Mbtu in 2011.
M.7.11	Demonstrate and validate non-ethanol fuels from lignin or waste biomass derived syngas
M.7.11.1	Demonstrate non-ethanol fuel production from lignin or biomass-derived syngas
M.7.11.2	Validate non-ethanol fuel separation
M.7.11.3	Validate integrated production of non-ethanol fuels from syngas at pilot scale
M.7.11.4	Validate integrated production of non-ethanol fuels from syngas at demonstration scale
M.7.12	Demonstrate and validate hydrogen production from lignin or waste biomass derived syngas
M.7.12.1	Demonstrate optimized hydrogen production from syngas
M.7.12.2	Validate hydrogen separation/recovery
M.7.12.3	Validate integrated production of hydrogen from syngas at pilot scale
M.7.12.4	Validate integrated production of hydrogen from syngas at demonstration scale
M.7.13	Demonstrate and validate product(s) from lignin or waste biomass derived syngas
M.7.13.1	Demonstrate high value chemical/material production from syngas
M.7.13.2	Validate product(s) separation
M.7.13.3	Validate integrated production of product(s) from syngas at pilot scale
M.7.13.4	Validate integrated production of product(s) from syngas at demonstration scale
M.7.14	Demonstrate and validate combined heat and power production from lignin or waste biomass derived syngas
M.7.14.1	Demonstrate combined heat and power production from syngas
M.7.14.2	Validate integrated production of heat and power from syngas at pilot scale
M.7.14.3	Validate integrated production of heat and power from syngas at demonstration scale
M.7.15	Demonstrate and validate waste biomass pyrolysis to produce pyrolysis oil intermediate
M.7.15.1	Validate feeder systems to reliably feed solid biomass to pyrolysis reactor high pressure (30 bar) systems
M.7.15.2	Validate pyrolysis performance

M.7.15.3	Validate pyrolysis oil cleanup performance
M.7.15.4	Validate capital costs
M.7.15.5	Validate integrated pyrolysis and pyrolysis oil cleanup at pilot scale
M.7.15.6	Validate integrated pyrolysis and pyrolysis oil cleanup at demonstration scale
M.7.15.7	Validate feed flexibility in integrated system
M.7.16	Demonstrate and validate fuels from pyrolysis oil intermediate
M.7.16.1	Demonstrate fuel production from pyrolysis oil intermediate
M.7.16.2	Validate fuel separation
M.7.16.3	Validate integrated production of fuels from pyrolysis oil at pilot scale
M.7.16.4	Validate integrated production of fuels from pyrolysis oil at demonstration scale
M.7.17	Demonstrate and validate high value chemical and material products from pyrolysis oil intermediates
M.7.17.1	Demonstrate high value chemical/material production from pyrolysis oil
M.7.17.2	Validate product separation
M.7.17.3	Validate integrated production of product(s)from pyrolysis oil at pilot scale
M.7.17.4	Validate integrated production of product(s)from pyrolysis oil at demonstration scale

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Ft. Myers, FL 33912

Future Algenol Facility

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Tenant's Initials REDACTED
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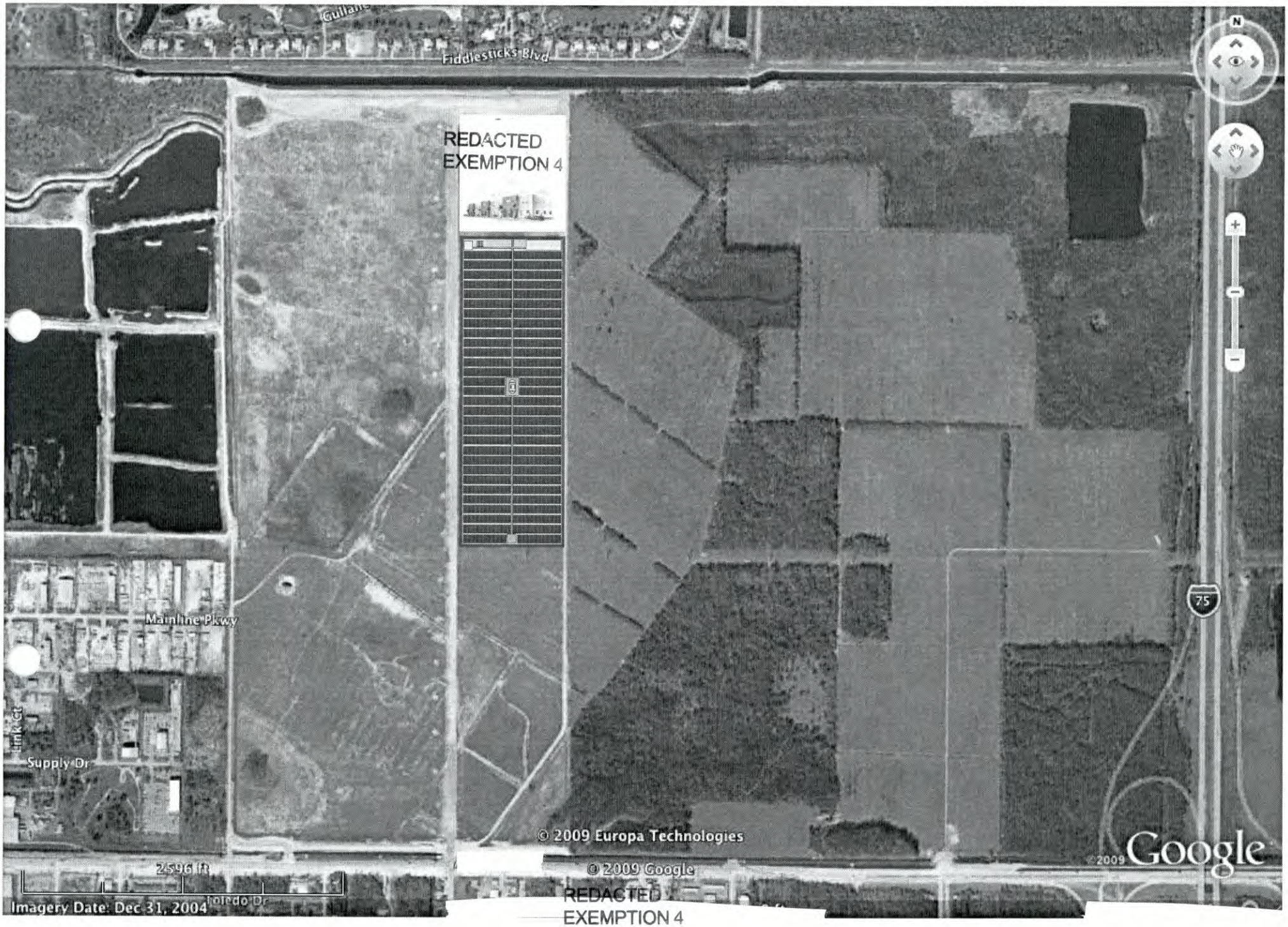

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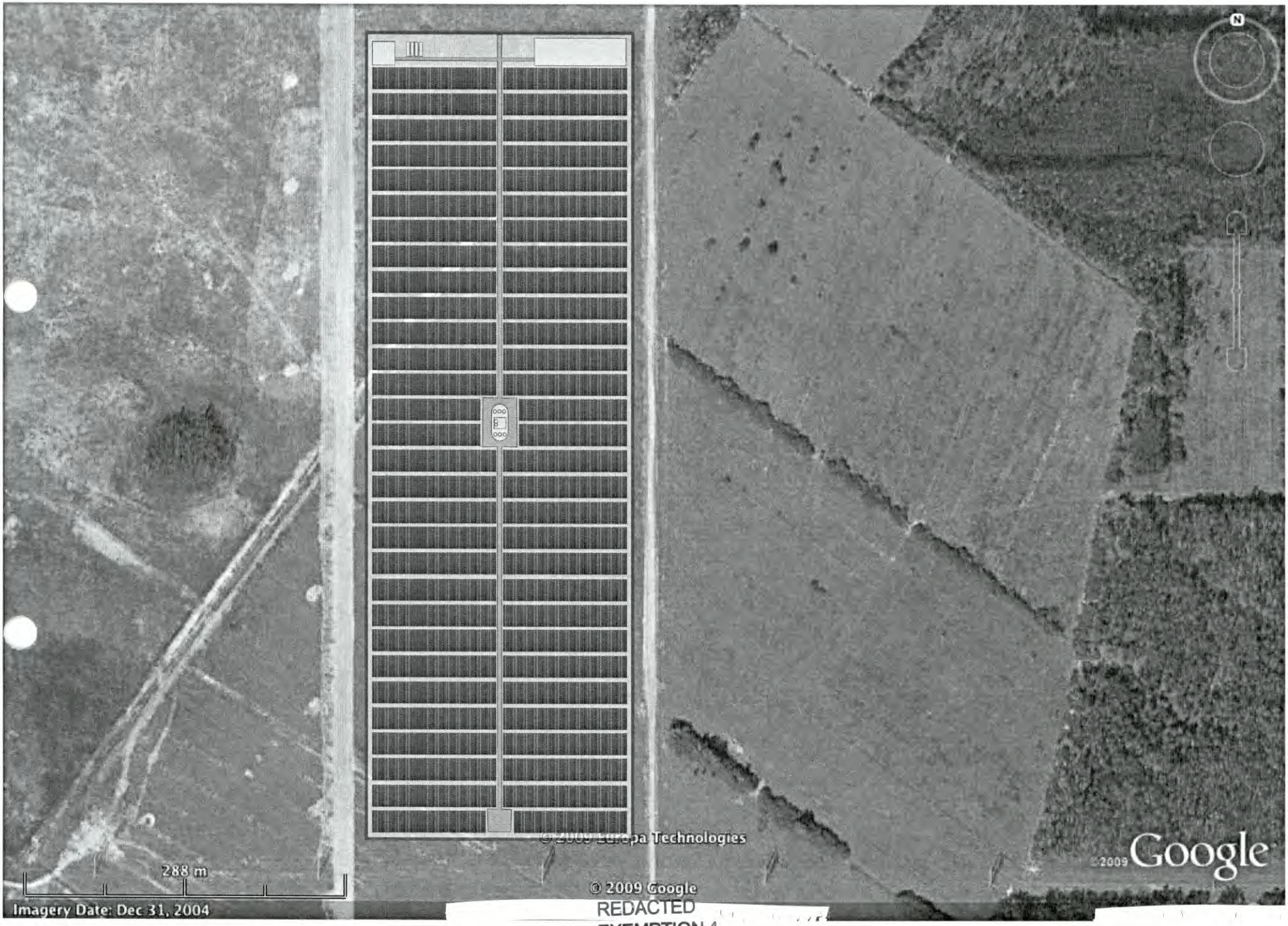

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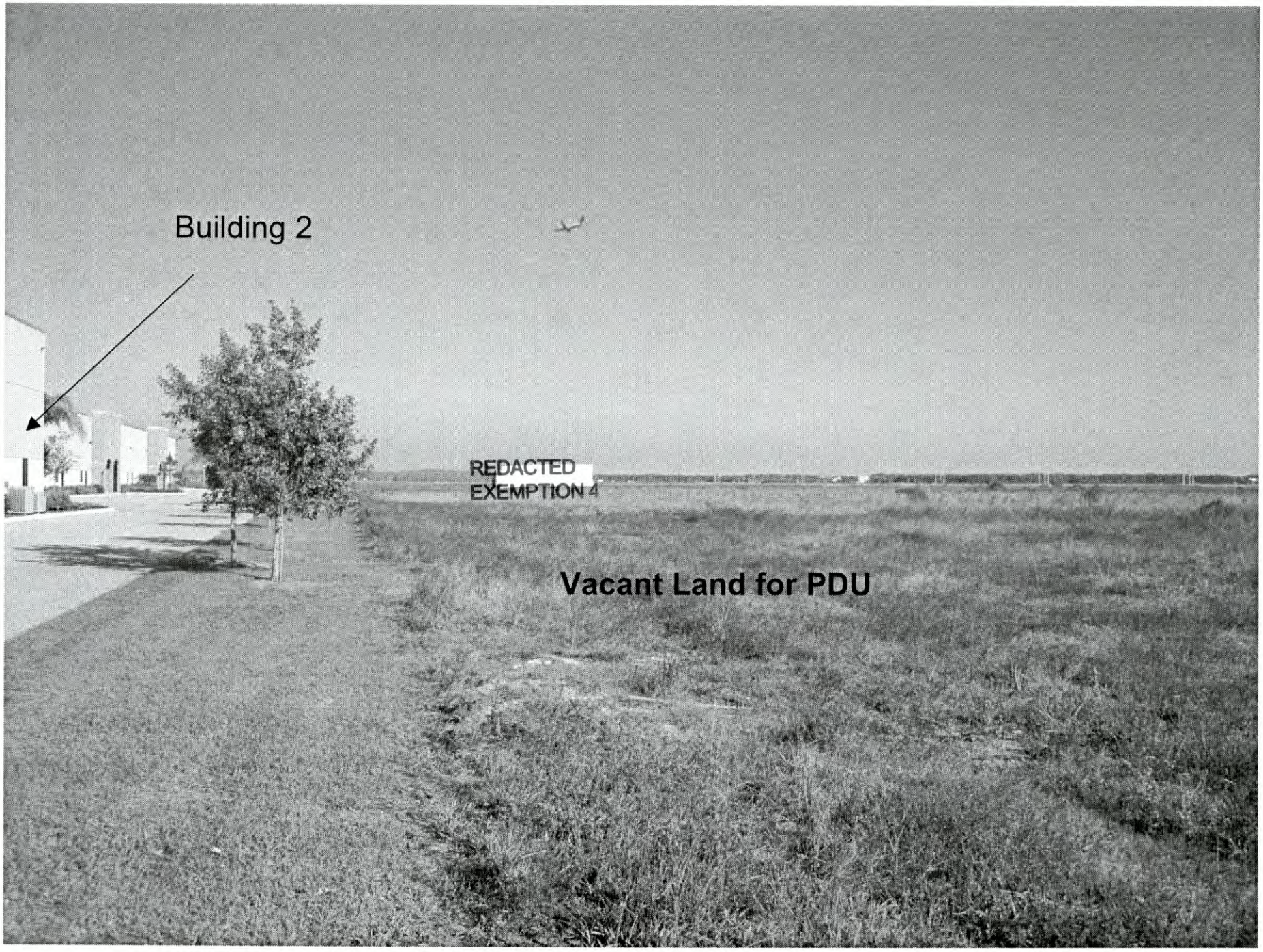
EXEMPTION 4

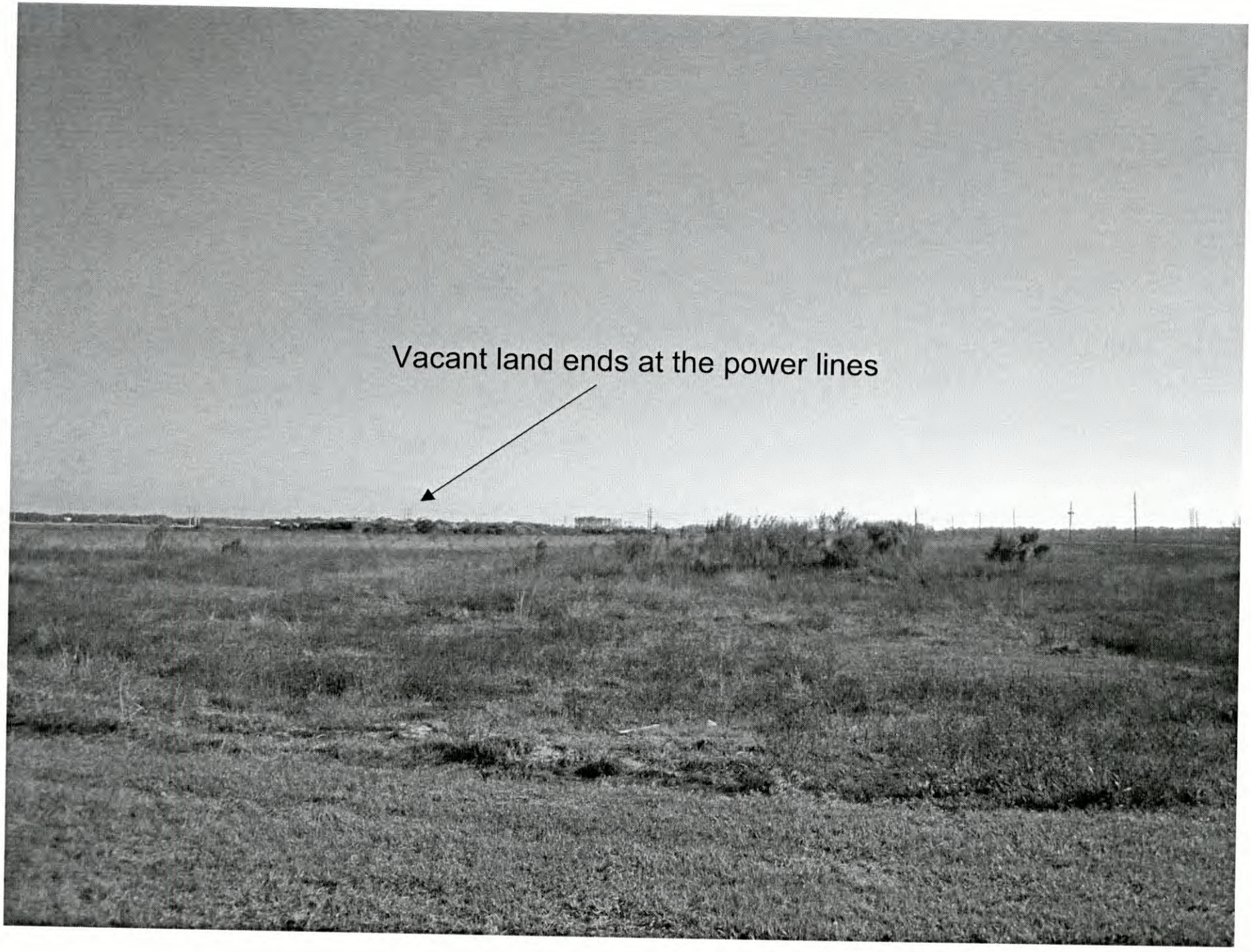
Front of Building 1

Future Lab and Office Area in Building 1

Future Lab and Office Area Building 2

Building 2 (Left) and Building 1 (Right)


Building 2
REDACTED
EXEMPTION 4
Vacant Land for PDU


Vacant land ends at the power lines

Attachment A: Resource Loaded Project Plan

ID	WBS	Task Name	Duration	Start	Finish	2009 Qtr 1	Qtr 2	Qtr 3	Qtr
1	**A**	Exemption 4							
2	A.1								
3	**A.2**								
4	**A.2.1**								
5	**A.2.1.1**								
6	A.2.1.1.1								
7	A.2.1.1.2								
8	A.2.1.1.3								
9	A.2.1.1.4								
10	**A.2.1.2**								
11	A.2.1.2.1								
12	A.2.1.2.2								
13	A.2.1.2.3								
14	A.2.1.2.4								
15	A.2.1.2.5								
16	**A.2.2**								
17	A.2.2.1								
18	A.2.2.2								
19	A.2.2.3								
20	A.2.2.4								
21	**A.2.3**								
22	A.2.3.1								
23	A.2.3.2								
24	A.2.3.3								
25	A.2.3.4								
26	A.2.3.5								
27	A.2.3.6								
28	**A.2.4**								
29	A.2.4.1								
30	**A.2.4.2**								
31	A.2.4.2.1								
32	A.2.4.2.2								
33	A.2.4.2.3								
34	A.2.4.2.4								
35	**A.3**								

ID	WBS	Task Name	Duration	Start	Finish	2009 Qtr 1	Qtr 2	Qtr 3	Qtr
36	**A.3.1**	Exemption 4							
37	A.3.1.1								
38	A.3.1.2								
39	A.3.1.3								
40	A.3.1.4								
41	A.3.1.5								
42	A.3.1.6								
43	A.3.1.7								
44	A.3.1.8								
45	A.3.1.9								
46	A.3.1.10								
47	**A.3.1.11**								
48	A.3.1.11.1								
49	A.3.1.11.2								
50	**A.3.2**								
51	A.3.2.1								
52	A.3.2.2								
53	A.3.2.3								
54	**A.3.3**								
55	A.3.3.1								
56	A.3.3.2								
57	A.3.3.3								
58	**A.4**								
59	**A.4.1**								
60	**A.4.1.1**								
61	A.4.1.1.1								
62	A.4.1.1.2								
63	A.4.1.1.3								
64	**A.4.1.2**								
65	A.4.1.2.1								
66	A.4.1.2.2								
67	A.4.1.2.3								
68	**A.4.1.3**								
69	A.4.1.3.1								
70	A.4.1.3.2								

ID	WBS	Task Name	Duration	Start	Finish	2009 Qtr 1	Qtr 2	Qtr 3	Qtr
71	A.4.1.3.3	Exemption 4							
72	**A.4.1.4**								
73	A.4.1.4.1								
74	A.4.1.4.2								
75	A.4.1.4.3								
76	**A.4.1.4.4**								
77	A.4.1.4.4.1								
78	A.4.1.4.4.2								
79	**A.4.1.5**								
80	A.4.1.5.1								
81	**A.4.1.5.2**								
82	A.4.1.5.2.1								
83	A.4.1.5.2.2								
84	**A.4.1.6**								
85	**A.4.1.6.1**								
86	A.4.1.6.1.1								
87	A.4.1.6.1.2								
88	A.4.1.6.1.3								
89	A.4.1.6.1.4								
90	**A.4.1.6.2**								
91	A.4.1.6.2.1								
92	A.4.1.6.2.2								
93	A.4.1.6.2.3								
94	**A.4.1.7**								
95	A.4.1.7.1								
96	A.4.1.7.2								
97	A.4.1.7.3								
98	A.4.1.7.4								
99	A.4.1.7.5								
100	A.4.1.7.6								
101	**A.4.2**								
102	**A.4.2.1**								
103	**A.4.2.1.1**								
104	A.4.2.1.1.1								
105	A.4.2.1.1.2								

ID	WBS	Task Name	Duration	Start	Finish	2009 Qtr 1	Qtr 2	Qtr 3	Qtr
106	A.4.2.1.1.3	Exemption 4							
107	A.4.2.1.1.4								
108	**A.4.2.1.2**								
109	A.4.2.1.2.1								
110	A.4.2.1.2.2								
111	A.4.2.1.2.3								
112	A.4.2.1.2.4								
113	**A.4.2.1.3**								
114	A.4.2.1.3.1								
115	A.4.2.1.3.2								
116	A.4.2.1.3.3								
117	A.4.2.1.3.4								
118	**A.4.2.1.4**								
119	A.4.2.1.4.1								
120	A.4.2.1.4.2								
121	A.4.2.1.4.3								
122	A.4.2.1.4.4								
123	**A.4.2.1.5**								
124	A.4.2.1.5.1								
125	A.4.2.1.5.2								
126	**A.5**								
127	**A.5.1**								
128	A.5.1.1								
129	**A.5.2**								
130	A.5.2.1								
131	A.5.2.2								
132	A.5.2.3								
133	**A.5.3**								
134	A.5.3.1								
135	A.5.3.2								
136	A.5.3.3								
137	A.5.3.4								
138	**A.6**								
139	A.6.1								
140	A.6.2								

ID	WBS	Task Name	Duration	Start	Finish	2009 Qtr 1	Qtr 2	Qtr 3	Qtr
141	A.6.3	Exemption 4							
142	A.6.4								
143	A.6.5								
144	A.6.6								
145	**A.7**								
146	A.7.1								
147	A.7.2								
148	A.7.3								
149	A.7.4								
150	**A.8**								
151	A.8.1								
152	A.9								
153	**A.10**								
154	A.10.1								
155	A.10.2								
156	A.11								
157	**B**								
158	**B.1**								
159	B.1.1								
160	B.1.2								
161	B.2								
162	B.3								
163	**B.4**								
164	B.4.1								
165	B.4.2								
166	B.4.3								
167	**B.5**								
168	**B.5.1**								
169	**B.5.1.1**								
170	B.5.1.1.1								
171	B.5.1.1.2								
172	B.5.1.1.3								
173	**B.5.1.2**								
174	B.5.1.2.1								
175	B.5.1.2.2								

ID	WBS	Task Name	Duration	Start	Finish	2009 Qtr 1	Qtr 2	Qtr 3	Qtr
176	B.5.1.2.3	Exemption 4							
177	B.5.1.2.4								
178	**B.5.1.3**								
179	B.5.1.3.1								
180	B.5.1.3.2								
181	B.5.1.3.3								
182	B.5.1.3.4								
183	B.5.1.3.5								
184	B.5.1.3.6								
185	**B.5.1.4**								
186	B.5.1.4.1								
187	B.5.1.4.2								
188	**B.5.1.5**								
189	B.5.1.5.1								
190	B.5.1.5.2								
191	B.5.2								
192	B.5.3								
193	**B.6**								
194	B.6.1								
195	B.6.2								
196	B.6.3								
197	B.6.4								
198	B.6.5								
199	**B.7**								
200	**B.7.1**								
201	B.7.1.1								
202	B.7.1.2								
203	**B.7.2**								
204	B.7.2.1								
205	B.7.2.2								
206	B.7.2.3								
207	**B.7.3**								
208	B.7.3.1								
209	B.7.3.2								
210	B.7.3.3								

ID	WBS	Task Name	Duration	Start	Finish	2009			
						Qtr 1	Qtr 2	Qtr 3	Qtr
211	B.7.3.4	Exemption 4							
212	B.7.3.5								
213	**B.7.4**								
214	B.7.4.1								
215	B.7.4.2								
216	B.7.4.3								
217	B.7.4.4								
218	B.7.4.5								
219	**B.7.5**								
220	**B.7.5.1**								
221	B.7.5.1.1								
222	B.7.5.1.2								
223	B.7.5.1.3								
224	B.7.5.1.4								
225	B.7.5.1.5								
226	**B.7.5.2**								
227	B.7.5.2.1								
228	B.7.5.3								
229	B.7.5.4								
230	B.7.5.5								
231	B.7.5.6								
232	B.7.5.7								
233	**B.7.6**								
234	**B.7.6.1**								
235	B.7.6.1.1								
236	B.7.6.1.2								
237	B.7.6.1.3								
238	B.7.7								
239	**B.8**								
240	**B.8.1**								
241	B.8.1.1								
242	**B.8.1.2**								
243	B.8.1.2.1								
244	**B.8.2**								
245	B.8.2.1								

ID	WBS	Task Name	Duration	Start	Finish	2009 Qtr 1	Qtr 2	Qtr 3	Qtr
246	B.8.2.2	Exemption 4							
247	**B.9**								
248	B.9.1								
249	**B.10**								
250	B.10.1								
251	**B.11**								
252	B.11.1								
253	B.11.2								
254	**C**								
255	**C.1**								
256	C.1.1								
257	**C.2**								
258	C.2.1								
259	C.2.2								
260	C.2.3								
261	C.2.4								
262	C.3								
263	C.4								
264	C.5								

Algenol Biofuels Inc.

Intellectual Property Statement

Background:

Algenol Biofuels Inc. is developing and commercializing Direct to Ethanol™ technology invented by Mr. Paul Woods and Dr. John Coleman between 1984 and 1996 and patented in the U.S. in 2001 and 2004 (US Patent Nos. 6,306,639 and 6,699,696). Direct to Ethanol™ technology involves over-expressing in blue-green algae (cyanobacteria) the genes for fermentation pathway enzymes (pyruvate decarboxylase and alcohol dehydrogenase). These enzymes are found widely in nature. The resulting enhanced algae actively carry out photosynthesis and utilize carbon dioxide, sunlight and water to make ethanol inside each algal cell. The ethanol made inside the cell diffuses through the cell wall into the culture medium and then evaporates, along with water, into the headspace of an enclosed, sealed photobioreactor designed by Algenol. The ethanol-water vapor is harvested from the photobioreactor, ethanol is separated from the ethanol-water vapor, and then condensed and distilled into fuel grade ethanol.

Algenol has assembled a team of more than 100 employees and consultants to develop the technology from proof-of-principle to commercialization, including molecular biologists, marine biologists, biochemists, mechanical and chemical engineers, project managers and two full time patent attorneys. Since inception, the Company has filed several provisional and non-provisional patent applications covering recent inventions in the field and expects to continue this practice for the foreseeable future. In addition to the technologies for which the Company has obtained, or is pursuing, a patent, it has amassed significant knowledge and trade secrets related to the above detailed Direct to Ethanol™ technology.

All of the IP necessary to complete this project is owned, and has been developed, by Algenol and its wholly owned subsidiaries. Rights to use, commercialize and license the technology reside solely with Algenol. The above referenced patents were originally assigned to Enol Energy Inc., a Company started by Mr. Woods, which has since become a wholly owned subsidiary of Algenol. The license agreements transferring the rights to the technology to Algenol grants exclusive, worldwide, royalty-free right and license to use, sell, manufacture and otherwise commercialize the technology. Mr. Woods, pursuant to the agreement, assigned his rights to the technology to Algenol. Below please find further details regarding Algenol's patents and patent applications.

Exemption 4

The following patents and patent applications are owned by Algenol:

Exemption 4

Exemption 4

In each instance, the inventors of the intellectual property that is the subject of these patents have either been an employee or a consultant of Algenol, or one of its wholly owned subsidiaries, at the time of the invention. Algenol's standard employment agreements and consulting agreements include the following language, or language substantially the same:

> **Proprietary Rights.** All work arising from the Services performed hereunder all materials and products developed or prepared for Company by Employee in connection with the Services performed hereunder, and all resulting inventions, discoveries, processes, ideas, methods, designs, know-how, whether or not patentable, and other copyrightable materials (all of the foregoing being referred to as "Work Product") are the exclusive property

throughout the world of Company, and all right, title and interest therein shall vest in Company and are hereby assigned to the Company. Whenever requested to do so by Company or any subsidiary and/or affiliate thereof, at Company's expense, and without further compensation or consideration, Consultant shall promptly execute any and all applications, assignments and other instruments and perform such acts which Company shall deem necessary or advisable in order to apply for and obtain copyrights, letters, patents and other applicable statutory

In addition to the above detailed patents and patent applications, Algenol has filed patent applications for these inventions in other jurisdictions, including Europe, Canada, and Australia.

As a distinct matter, Algenol Biofuels, Inc. has been granted an exclusive license by the University of Hawaii to rights in PCT/US2007/001071 ["Methods and Compositions for Ethanol Producing Cyanobacteria"], and national stage applications derived therefrom. Allowance of claims is soon expected in the European counterpart, EP 1979481.

Discussion:

Exemption 4

Exemption 4

ALGENOL
BIOFUELS
HARNESSING THE SUN TO FUEL THE WORLD

March 12, 2010

Christine M. English, Ph.D.
Senior Project Engineer, Biomass
Navarro Research and Engineering, Inc.
U.S. DOE Golden Field Office
1617 Cole Blvd.
Golden, CO 80401

Dear Dr. English:

REDACTED
EXEMPTION 5
- deliberative process
- attorney-client privilege

Sincerely yours,

Lawrence B. Ebert

Lawrence B. Ebert, J.D., Ph.D.
Registered patent attorney
Phone 908-938-1660

The Dow Chemical Company
2301 N. Brazosport Blvd
Freeport, Texas 77541-3257
USA

Certified Letter #

REDACTED
EXEMPTION 4

February 22, 2010

Craig R. Smith, M.D.
Chief Operating Officer
Algenol Biofuels Inc.

Estimate of Property Value for Industrial Lease

Dear Craig,

This letter is in response to the request for a description of the methodology that The Dow Chemical Company ("Dow") used to estimate the property value of land for the

REDACTED
EXEMPTION 4

Best regards,

Doug Whipple
Property Management
Texas Operations

Algenol Biofuels Inc.

Intellectual Property Statement

Background:

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Exemption 4

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Exemption 4

Exemption 4

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> **Proprietary Rights.** All work arising from the Services performed hereunder all materials and products developed or prepared for Company by Employee in connection with the Services performed hereunder, and all resulting inventions, discoveries, processes, ideas, methods, designs, know-how, whether or not patentable, and other copyrightable materials (all of the foregoing being referred to as "Work Product") are the exclusive property throughout the world of Company, and all right, title and interest therein shall vest in Company and are hereby assigned to the Company. Whenever requested to do so by Company or any subsidiary and/or affiliate thereof, at Company's expense, and without further compensation or consideration, Consultant shall promptly execute any and all applications, assignments and other instruments and perform such acts which Company shall

deem necessary or advisable in order to apply for and obtain copyrights, letters, patents and other applicable statutory

In addition to the above detailed patents and patent applications, Algenol has filed patent applications for these inventions in international jurisdictions, including Europe, Canada, Australia and the World Intellectual Property Organization.

Discussion:

Exemption 4

Exemption 4

Project Management Plan – Statement of Work

Pilot-Scale Integrated Biorefinery Operations for Producing Ethanol From Algae

Algenol Biofuels Inc.

Narrative of WBS Tasks

Exemption
4

Exemption 4

Exemption 4

Exemption 4

Exemption 4

Exemption 4

Exemption 4

Exemption 4

Exemption 4

Exemption 4

Exemption 4

Exemption 4

Exemption 4

Exemption 4

Gate Review Descriptions

Phase I - The Phase I gate criteria will be finalized as part of the negotiation of the final award instrument. Phase I Gate Criteria will be proposed by the Project Management Team (PMT) at the initiation of the project, approved by the Internal Gatekeeper Team (IGT), and communicated to DOE. At a minimum, at the completion of Phase I, the internally defined Gate Criteria for Phase I will require:

Exemption 4

Exemption 4

Identification of Roles and Responsibilities

One of Algenol's Specific Aims in this project is to assemble a consortium of private industry, federal laboratories, and academic institutions that will contribute to the development and operation of the Algenol pilot-scale integrated biorefinery. Algenol has accomplished this goal by signing collaborative agreements with The Dow Chemical Company, The National Renewable Energy Laboratory (NREL), Membrane Technology & Research Inc. (MTR), and The Georgia Tech Strategic Energy Institute, a division of The Georgia Institute of Technology (Georgia Tech). Exemption 4

Significantly, Dow will: 1) lease to the Company 29 acres of land on Dow's chemical plant in Freeport, Texas, 2) lead in the development of advanced materials for use in the flexible film photobioreactors with requirements for those materials being delivered by Algenol, 3) evaluate various ethanol-water separation technologies and strategies, 4) evaluate and test various water treatment, handling and disposal options for water, 5) provide engineering, analytical, EH&S, and administrative support, including access to Dow manuals and procedures relating to EH&S and assistance in complying with such procedures, and 6) supply all saltwater and fresh water and other utility services.

As a component of this proposal, NREL will: 1) conduct simulated laboratory and on-site analysis of coal and natural gas power plant flue gas, as well as industrial sources of carbon dioxide emissions, and their impacts on Algenol algae samples, 2) develop an Aspen Plus techno-economic model, including mass and energy balances, for Algenol's Direct to Ethanol™ process Exemption 4

Georgia Tech will also be a significant collaborator on the project. Specifically, Georgia Tech will: 1) develop technologies and processes for delivering carbon dioxide to the algae and separating carbon dioxide from other gases, 2) develop technologies and processes for extracting oxygen from the headspace of the photobioreactor, 3) design and test ethanol separation technologies, in collaboration with the University of Colorado, that increase the ethanol concentration from a dilute stream to pure ethanol, and 4) refine the analysis of the life-cycle environmental impacts of Algenol's process included in this proposal.

*MTR will: Exemption 4

Project Management and Organizational Control

II. Management Organization and Responsibilities

This project will be managed by a series of hierarchical teams designed to oversee the WBS for each Phase. After each gate review, the structure and composition of the teams will be adapted to the tasks and activities for the new Phase. At the initiation of the project, the team structure will be as follows:

Figure 1. Program Team Organizational Structure

Exemption 4

Exemption 4

Exemption 4

Exemption 4

Phase I Risk Management Plan

Algenol Biofuels Inc.

March 12, 2009

The Phase I Risk Management Plan (Phase I RMP) for the program defines the scope and process for the identification, assessment, and management of risks that could alter the implementation of the program. The Phase I RMP includes assessable risks that could potentially jeopardize successful completion of the project's Phase I technical and environmental goals. The objective of this plan is to define the strategy to manage program-related risks throughout the project life cycle such that there is acceptable minimal impact on cost and schedule, as well as operational performance. The Phase I RMP follows DOE Order 413.3 and its associated guidance on program and project management principles. The RMP is considered a living document which will be updated as needed to ensure that previously identified risks are managed effectively and new risks are quickly identified and managed throughout the life cycle.

The Program Management Team will review the risk analysis report and will be responsible for reviewing the identified project risks, developing risk mitigation strategies, and overseeing implementation of risk mitigation techniques. Project team members will be responsible for execution of risk mitigation strategies and techniques.

Risks are assessed as low, moderate or high. Low risk means a 25% or less probability of failure. Moderate risk means a 26% to 50% probability of failure. High risk means greater than a 50% probability of failure.

The current Phase I project-related risks are:

Technical Risks:

1. Failure to achieve the targeted ethanol productivity of the hybrid algae.

Exemption 4